

## **REMARKS**

By the present amendment, claims 1-3 and 5 are pending in the application. Claims 1 and 5 are independent. Claim 4 is cancelled, the contents of which have been incorporated into independent claim 1.

### **Support for claim amendments**

Claim 1 has been amended to recite “by means of bringing the gas produced at the time of compression shaping the waste plastic into contact with water or ammonia solution and combining the water or ammonia solution with an ammonia solution of an ammonia solution treatment facility attached to a coke oven.” Support for the claim amendment is found at page 5, lines 20-24, and at page 13, lines 2-24.

### **§ 102/§ 103**

**Claims 1-3 are rejected under 35 U.S.C. § 102(b) as being anticipated by JP 2001 -49261 and claims 1-5 are rejected under 35 U.S.C. 103(a) as being unpatentable over JP 2001 -49261 in view of Uematsu et al.** These rejections are respectfully traversed for at least the reasons set forth below.

The technology disclosed in the '261 patent relates to a method for reutilizing waste plastic and waste plastic processing method, where the method for attaining a fuel gas, liquefied product, and coke by effecting dry distillation in a coke oven as the method for recycling scrap plastics generated in the plastic processing steps and used plastics to be recovered, and plastics granulated to have an apparent specific gravity of 0.40-0.95 kg/liter are subjected to dry distillation in a coke oven, and further, plastics with a reduced mixed ash content are used. See, Abstract.

In the presently claimed invention, a gas produced at the time of compression shaping of the molten waste plastic is brought into contact with water or an ammonia solution. However, the '261 patent does not remove the chlorine components by bringing the thermally decomposed chlorine based gas emitted during treatment of the waste plastic into contact with aqueous ammonia. In addition, the '261 patent describes that melting plastic temperature is 100-160°C, which is different temperature of the present invention, and apparent specific density is 0.40-0.95 kg/liter, which is different from 0.7 to 1.2 kg/liter. As

described above, the '261 patent only describes a method for obtaining a fuel gas, a liquefied product, and coke by effecting dry distillation in a coke oven as the method for recycling scrap plastics. Therefore, the '261 patent does not teach or suggest the present inventive features.

The invention disclosed in the Uematsu patent relates to a method of presorting waste plastics according to chlorine content. Specifically, waste plastics with a high chlorine content that have been separated and excluded for blast furnace use, or waste plastics that have not been thoroughly treated in the blast furnace, may be subjected to high-temperature decomposition in a thermal decomposition treatment furnace for gasification, such as a partial oxidation furnace or dry distillation oven, provided with the blast furnace. Any type of furnace may be employed so long as the atmosphere is reducing and the temperature is at least 400°C which allows gasification of the waste plastics. See, column 12, lines 44-49. In contrast, the presently claimed invention specifies the temperature range of 160°C to 250°C. Therefore, the Uematsu patent does not teach or suggest the present inventive features.

Thus, the '261 patent and the Uematsu patent, either alone or in combination, do not render the claimed invention anticipated or obvious. It is therefore submitted that amended claims 1-3 and 5 are patentable. Applicants respectfully request reconsideration and withdrawal of the rejection of claims 1-3 and 5 over the '261 patent and the Uematsu patent under 35 U.S.C. § 102(b) and § 103(a).

### CONCLUSION

It is submitted that in view of the present amendment and foregoing remarks, the application is now in condition for allowance. It is therefore respectfully requested that the application, as amended, be allowed and passed for issue.

Respectfully submitted,

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